# CHEATHERO SHEETSHERO

A comprehensive cheat sheet covering essential concepts and formulas in Chemical Engineering, useful for quick reference and exam preparation.



# Thermodynamics

#### Fundamental Concepts

# Equations of State

| First Law of<br>Thermodynamics  | <ul> <li>ΔU = Q - W</li> <li>ΔU: Change in<br/>internal energy</li> <li>Q: Heat added to the<br/>system</li> <li>W: Work done by the<br/>system</li> </ul> | Ideal Gas Law  | <ul> <li>PV = nRT</li> <li>P: Pressure</li> <li>V: Volume</li> <li>n: Number of moles</li> <li>R: Ideal gas constant</li> <li>T: Temperature</li> </ul> |  |
|---------------------------------|--|--|---|--|
| Enthalpy (H)                    | H = U + PV<br>• U: Internal energy<br>• P: Pressure  | Van der Waals<br>Equation  | <ul> <li>(P + a(n/V)<sup>2</sup>)(V - nb) = nRT</li> <li>a, b: Van der Waals<br/>constants</li> </ul>   |  |
|                                 | • v. volume  | Peng-Robinson  | $P = (RT)/(V_m - b) -$  |  |
| Second Law of<br>Thermodynamics | ΔS ≥ 0 (for a closed<br>system)<br>• ΔS: Change in<br>entropy  | Equation   | <ul> <li>V_m: Molar volume</li> <li>a, b, α: Peng-Robinson parameters</li> </ul>  |  |
| Gibbs Free Energy G = H - TS    |  | Thermodynamic Cycles   |   |  |
| (G)                             | <ul> <li>T: Temperature</li> <li>S: Entropy</li> <li>At constant T and P,<br/>ΔG &lt; 0 for a<br/>spontaneous process.</li> </ul>                          | Carnot         η = 1           Cycle         • r           • 1         • 7 | - (Tc/Th)<br>ŋ: Efficiency<br>Гc: Cold reservoir temperature<br>Гh: Hot reservoir temperature   |  |
| Helmholtz Free<br>Energy (A)    | <ul> <li>A = U - TS</li> <li>At constant T and V,</li> <li>ΔA &lt; 0 for a spontaneous process.</li> </ul>   | Rankine Used<br>Cycle Inclue<br>cond                                       | in steam power plants.<br>des pump, boiler, turbine, and<br>enser.  |  |
| Heat Capacity                   | Cv = (∂U/∂T)v<br>Cp = (∂H/∂T)p   |  |   |  |

## **Fluid Mechanics**

#### Fluid Properties

# Fluid Statics

| Density (ρ)            | ρ = m/V<br>• m: Mass<br>• V: Volume                       |
|------------------------|---|
| Viscosity (µ)          | Measure of a fluid's resistance to flow.                  |
| Surface<br>Tension (σ) | Energy required to increase the surface area of a liquid. |
|                        |   |

| Pressure (P)            | P = F/A<br>• F: Force<br>• A: Area   |
|-------------------------|--|
| Hydrostatic<br>Pressure | <ul> <li>P = ρgh</li> <li>ρ: Density</li> <li>g: Acceleration due to gravity</li> <li>h: Height</li> </ul> |
| Buoyancy                | Archimedes' principle: Buoyant<br>force equals the weight of the<br>fluid displaced.                       |

#### Fluid Dynamics

| Continuity<br>Equation     | <ul> <li>A1V1 = A2V2 (for</li> <li>incompressible fluids)</li> <li>A: Cross-sectional area</li> <li>V: Velocity</li> </ul>  |
|----------------------------|---|
| Bernoulli's<br>Equation    | <ul> <li>P + (1/2)pV^2 + pgh = constant</li> <li>P: Pressure</li> <li>p: Density</li> <li>V: Velocity</li> <li>g: Acceleration due to<br/>gravity</li> <li>h: Height</li> </ul> |
| Navier-Stokes<br>Equations | Equations describing the motion of viscous fluid substances.  |
| Reynolds<br>Number (Re)    | <ul> <li>Re = (pVD)/µ</li> <li>p: Density</li> <li>V: Velocity</li> <li>D: Diameter</li> <li>µ: Viscosity</li> </ul>  |
| Friction Factor<br>(f)     | Used to calculate pressure drop in pipes.   |

### Mass Transfer

#### Diffusion

#### Distillation

| Fick's First Law J =   | J = -D (dC/dx)<br>• J: Diffusion flux<br>• D: Diffusion coefficient<br>• C: Concentration<br>• x: Distance<br>w ∂C/∂t = D (∂ <sup>2C/∂x</sup> 2) | Relative<br>Volatility (α) | <ul> <li>α = (yA/xA) / (yB/xB)</li> <li>yA, yB: Vapor mole<br/>fractions of components A<br/>and B</li> <li>xA, xB: Liquid mole<br/>fractions of components A<br/>and B</li> </ul> | Stripping Factor<br>(S) | <ul> <li>S = (mG)/L</li> <li>m: Slope of equilibrium line</li> <li>G: Gas flow rate</li> <li>L: Liquid flow rate</li> </ul> |
|--|--|----------------------------|--|-------------------------|---|
|  | <ul><li>C: Concentration</li><li>t: Time</li></ul>   | McCabe-<br>Thiele Method   | Graphical method for designing distillation columns.   |                         |   |
| <ul> <li>D: Diffusion coeffici</li> <li>x: Distance</li> </ul> | <ul> <li>D: Diffusion coefficient</li> <li>x: Distance</li> </ul>  | Fenske<br>Equation         | N_min = log( (xA,D/xB,D) *<br>(xB,B/xA,B) ) / log(α)<br>• N_min: Minimum number of   |                         |   |
| Mass Transfer Coefficient                                      |  |                            | <ul> <li>xA,D, xB,D: mole fractions</li> </ul>   |                         |   |
| Mass Transfer  | Relates the mass transfer rate   |                            | of A and B in distillate   |                         |   |

• xA,B, xB,B: mole fractions of A and B in bottoms

Absorption

| Mass Transfer   | Relates the mass transfer rate                       |  |
|-----------------|--|--|
| Coefficient (k) | to the concentration                                 |  |
|                 | difference.  |  |
|                 | N = k∆C  |  |
|                 | N: Mass transfer rate                                |  |
|                 | <ul> <li>k: Mass transfer<br/>coefficient</li> </ul> |  |
|                 | <ul> <li>ΔC: Concentration<br/>difference</li> </ul> |  |

# **Chemical Reaction Engineering**

| Reaction Kinetics     |  |  |
|-----------------------|--|--|
| Rate Law              | <ul> <li>-rA = k CA<sup>n</sup></li> <li>-rA: Rate of disappearance of reactant A</li> <li>k: Rate constant</li> <li>CA: Concentration of A</li> <li>n: Order of reaction</li> </ul> |  |
| Arrhenius<br>Equation | <ul> <li>k = A exp(-Ea/RT)</li> <li>k: Rate constant</li> <li>A: Pre-exponential factor</li> <li>Ea: Activation energy</li> <li>R: Gas constant</li> <li>T: Temperature</li> </ul>   |  |

| Reactor | Types |
|---------|-------|
| reactor | 19000 |

#### or Types

| Batch Reactor                                | Closed system; reactants<br>are mixed and allowed to<br>react for a certain time. |
|--|---|
| Continuous<br>Stirred-Tank<br>Reactor (CSTR) | Continuous flow of<br>reactants and products;<br>perfectly mixed.                 |
| Plug Flow Reactor<br>(PFR)                   | Continuous flow; no mixing in the axial direction.                                |

#### Reactor Design Equations

| CSTR Design<br>Equation | <ul> <li>V = (FAO XA) / (-rA)</li> <li>V: Reactor volume</li> <li>FAO: Molar flow rate of A at inlet</li> <li>XA: Conversion of A</li> <li>-rA: Rate of disappearance of A</li> </ul>   |
|-------------------------|---|
| PFR Design<br>Equation  | <ul> <li>V = f(FAO dXA) / (-rA)</li> <li>V: Reactor volume</li> <li>FAO: Molar flow rate of A at inlet</li> <li>XA: Conversion of A</li> <li>-rA: Rate of disappearance of A</li> <li>Integration is performed over the range of conversion.</li> </ul> |